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(FILE 'HOME' ENTERED AT 12:39:26 ON 23 MAR 2009)

FILE 'CAPLUS' ENTERED AT 12:39:37 ON 23 MAR 2009

L1 14734 S (PHARMACEUTICAL OR PHARMACEUTICALS) (L) (PULVERIZE OR PULVERIZA  
L2 49 S L1 AND (JET MILL)

=> d que l2 stat

L1 14734 SEA FILE=CAPLUS ABB=ON PLU=ON (PHARMACEUTICAL OR PHARMACEUTIC  
ALS) (L) (PULVERIZE OR PULVERIZATION OR MILLING OR (JET MILL) OR  
POWDER)

L2 49 SEA FILE=CAPLUS ABB=ON PLU=ON L1 AND (JET MILL)

=> d l-49 bib abs

12 NUMBER 1 OF 49 CAPSULES OFFPRINT 2009 ACS on STN

AN 2009-141686 CAPSULE

13 Infusions of films and crystal properties on particle fracture in a jet mill

14 de Wael, Omer; Vromen, Herman; den Toonder, Jaap; van der Voort

15 Marshallville, Rect

16 Department of Mechanical Engineering, WU Osnabrueck, part of Schering-Plough

17 Corporation, Osn, 15400 Bldg, Neth

18 Powder Technology Center, 15400 Bldg, 72-77

19 Osnabrueck, PO Box 0002-0200

20 Elsevier B.V.

21 Journal

22 English

23 AB

Jet milling is commonly used for reducing the particle size of active pharmaceutical ingredients. Unfortunately, this process is sometimes difficult to control as pre-existing flaws and mesh properties affect the particle fracture behavior in a jet mill. In this study the effect of pre-existing flaws on mesh material properties of crystals of a model material, sodium chloride, from different sources have been investigated using optical microscopy, nanohardness, and powder compression. Subsequently, these properties have been correlated with particle fracture in a jet mill. The paper shows that pre-existing particles that have a small average flaw size possess the lowest constraint factor (i.e., the constraint factor is defined as the ratio of the hardness and the yield pressure) and is an extension of the ductility of the material; species materials that have a larger average flaw size have a high constraint factor and hence behave more ductile. Moreover, the study shows that the rank orders of the mesh properties are consistent with the rank order of the small determined particle size of breakers. Materials that have a relatively low hardness show the highest particle rate of breakage. The degree of particle fracture during jet-milling tends to decrease for particles that have a smaller flaw size and behave more ductile. The paper shows that pre-existing flaws have an impact on mesh properties and on particle fracture behavior in a jet mill. It is concluded that the increase of the particle rate of breakage as a function of particle size is influenced by the number of flaws rather than by flaw length.

12 NUMBER 2 OF 49 CAPSULES OFFPRINT 2009 ACS on STN

AN 2009-141686 CAPSULE

24 150-112774

25 Monomeric of polyols

26 Gerson, Michel Henri; Aude, Stouff, Robert Henri Marcel

27 PCT Int. Appl. 1999

28 Osnabrueck, Fixed

29 Patent

30 English

31 PAN ONT

32 PATENT NO

33 KIND

34 DATE

35 APPLICATION NO

36 DATE

37 PI 99 2000006130

38 A1 2000006130

39 W2 2000-0710854

40 2000071085

41 A1 2000071085

42 A2 2000071085

43 A3 2000071085

44 A4 2000071085

45 A5 2000071085

46 A6 2000071085

47 A7 2000071085

48 A8 2000071085

49 A9 2000071085

50 A10 2000071085

51 A11 2000071085

52 A12 2000071085

53 A13 2000071085

54 A14 2000071085

55 A15 2000071085

56 A16 2000071085

57 A17 2000071085

58 A18 2000071085

59 A19 2000071085

60 A20 2000071085

61 A21 2000071085

62 A22 2000071085

63 A23 2000071085

64 A24 2000071085

65 A25 2000071085

66 A26 2000071085

67 A27 2000071085

68 A28 2000071085

69 A29 2000071085

70 A30 2000071085

71 A31 2000071085

72 A32 2000071085

73 A33 2000071085

74 A34 2000071085

75 A35 2000071085

76 A36 2000071085

77 A37 2000071085

78 A38 2000071085

79 A39 2000071085

80 A40 2000071085

81 A41 2000071085

82 A42 2000071085

83 A43 2000071085

84 A44 2000071085

85 A45 2000071085

86 A46 2000071085

87 A47 2000071085

88 A48 2000071085

89 A49 2000071085

90 A50 2000071085

91 A51 2000071085

92 A52 2000071085

93 A53 2000071085

94 A54 2000071085

95 A55 2000071085

96 A56 2000071085

97 A57 2000071085

98 A58 2000071085

99 A59 2000071085

100 A60 2000071085

101 A61 2000071085

102 A62 2000071085

103 A63 2000071085

104 A64 2000071085

105 A65 2000071085

106 A66 2000071085

107 A67 2000071085

108 A68 2000071085

109 A69 2000071085

110 A70 2000071085

111 A71 2000071085

112 A72 2000071085

113 A73 2000071085

114 A74 2000071085

115 A75 2000071085

116 A76 2000071085

117 A77 2000071085

118 A78 2000071085

119 A79 2000071085

120 A80 2000071085

121 A81 2000071085

122 A82 2000071085

123 A83 2000071085

124 A84 2000071085

125 A85 2000071085

126 A86 2000071085

127 A87 2000071085

128 A88 2000071085

129 A89 2000071085

130 A90 2000071085

131 A91 2000071085

132 A92 2000071085

133 A93 2000071085

134 A94 2000071085

135 A95 2000071085

136 A96 2000071085

137 A97 2000071085

138 A98 2000071085

139 A99 2000071085

140 A100 2000071085

141 A101 2000071085

142 A102 2000071085

143 A103 2000071085

144 A104 2000071085

145 A105 2000071085

146 A106 2000071085

147 A107 2000071085

148 A108 2000071085

149 A109 2000071085

150 A110 2000071085

151 A111 2000071085

152 A112 2000071085

153 A113 2000071085

154 A114 2000071085

155 A115 2000071085

156 A116 2000071085

157 A117 2000071085

158 A118 2000071085

159 A119 2000071085

160 A120 2000071085

161 A121 2000071085

162 A122 2000071085

163 A123 2000071085

164 A124 2000071085

165 A125 2000071085

166 A126 2000071085

167 A127 2000071085

168 A128 2000071085

169 A129 2000071085

170 A130 2000071085

171 A131 2000071085

172 A132 2000071085

173 A133 2000071085

174 A134 2000071085

175 A135 2000071085

176 A136 2000071085

177 A137 2000071085

178 A138 2000071085

179 A139 2000071085

180 A140 2000071085

181 A141 2000071085

182 A142 2000071085

183 A143 2000071085

184 A144 2000071085

185 A145 2000071085

186 A146 2000071085

187 A147 2000071085

188 A148 2000071085

189 A149 2000071085

190 A150 2000071085

191 A151 2000071085

192 A152 2000071085

193 A153 2000071085

194 A154 2000071085

195 A155 2000071085

196 A156 2000071085

197 A157 2000071085

198 A158 2000071085

199 A159 2000071085

200 A160 2000071085

201 A161 2000071085

202 A162 2000071085

203 A163 2000071085

204 A164 2000071085

205 A165 2000071085

206 A166 2000071085

207 A167 2000071085

208 A168 2000071085

209 A169 2000071085

210 A170 2000071085

211 A171 2000071085

212 A172 2000071085

213 A173 2000071085

214 A174 2000071085

215 A175 2000071085

216 A176 2000071085

217 A177 2000071085

218 A178 2000071085

219 A179 2000071085

220 A180 2000071085

221 A181 2000071085

222 A182 2000071085

223 A183 2000071085

224 A184 2000071085

225 A185 2000071085

226 A186 2000071085

227 A187 2000071085

228 A188 2000071085

229 A189 2000071085

230 A190 2000071085

231 A191 2000071085







12 NUMBER 16 OF 49 CAPSULE OXYRIGHT 2009 ACS ON STN

AN 2007-140066 CAPSULE

IN 146-125459

TI New powder inhaled formulations of interferon

IN Tianjin, Hongqiao, Tian, Jiang, Zhang, Chongqing, Tian, Jiang

PA Tianjin Institute of Pharmaceutical Research, P.R. Rep. China

PO Peking Shuang Shengong Shuangong Shuangong, App.

COOBY CHINESE

JP Patent

LA Chinese

PAN CNT

FI IN 2006-160197 A 2006-09-08 CN 2006-160197 20060506  
 AB The invention provides new powder inhaled formulations of interferon. The interferon powder inhalation is composed of 0.0000-0.05 wt% of interferon, 0.00-0.05 wt% of diluting agent, 0.00-0.05 wt% of protective agent for protecting the activity of interferon, 0-20 wt% of adjuvant for improving dispersibility, and a salt buffer system for keeping pH at 4-8, wherein the interferon is selected from recombinant human interferon  $\alpha$ -2a, recombinant human interferon  $\alpha$ -2b, recombinant interferon  $\beta$ , and recombinant interferon  $\gamma$ , and the protective agent is selected from lysine, 2-hydroxypropyl- $\beta$ -cyclodextrin, and urethane lecithin. The product is free of absorption retardant and human serum albumin (HSA). The preparation method comprises the steps of mixing all ingredients, removing water content from the mixture by evaporation, and performing milling with a jet mill or ball mill or alternatively spray drying to obtain particles with an average grain size of less than 10  $\mu$ m.

12 NUMBER 17 OF 49 CAPSULE OXYRIGHT 2009 ACS ON STN

AN 2007-140068 CAPSULE

IN 146-125459

TI Pharmaceutical compositions of epidermone

IN Baidouk, Vaidouk, Baidouk, Baidouk, V. S. Choudhary, Q. N. Sharma, N. S.

PA Baidouk Pharmaceuticals Limited, India

PO PCT Int. Appl. 23pp.

COOBY FINISH

JP Patent

LA English

PAN CNT

FI IN 2006-160199 A 2006-09-08 IN 2006-160199 20060506  
 AB The invention provides new powder inhaled formulations of interferon. The interferon powder inhalation is composed of 0.0000-0.05 wt% of interferon, 0.00-0.05 wt% of diluting agent, 0.00-0.05 wt% of protective agent for protecting the activity of interferon, 0-20 wt% of adjuvant for improving dispersibility, and a salt buffer system for keeping pH at 4-8, wherein the interferon is selected from recombinant human interferon  $\alpha$ -2a, recombinant human interferon  $\alpha$ -2b, recombinant interferon  $\beta$ , and recombinant interferon  $\gamma$ , and the protective agent is selected from lysine, 2-hydroxypropyl- $\beta$ -cyclodextrin, and urethane lecithin. The product is free of absorption retardant and human serum albumin (HSA). The preparation method comprises the steps of mixing all ingredients, removing water content from the mixture by evaporation, and performing milling with a jet mill or ball mill or alternatively spray drying to obtain particles with an average grain size of less than 10  $\mu$ m.

AB This invention relates to alendronate antineoplastic particles such as epidermone particles having a 1000 particle size of less than 25  $\mu$ m and greater than 10  $\mu$ m are provided. Also provided are pharmaceutical compositions, containing the alendronate antineoplastic particles. Thus, epidermone was micronized by being passed through a spiral jet mill at a feed rate of about 100 g/h using a compressed air pressure of 4 kg/cm<sup>2</sup> to 6 kg/cm<sup>2</sup>. The micronized epidermone obtained was measured for its particle size through a Malvern particle size analyzer. The 90% of the epidermone particles was 16-17  $\mu$ m.

RE. CNT 4 THERE ARE 4 CITED REFERENCES AVAILABLE FOR THIS RECORD  
 ALL CITATIONS AVAILABLE IN THE RE. FORM

12 NUMBER 18 OF 49 CAPSULE OXYRIGHT 2009 ACS ON STN

AN 2007-172300 CAPSULE

IN 146-125459

TI New oral nanoparticle formulation of mast of Colloidal emulsion

IN Tian, Hongqiao, Tian, Jiang, Zhang, Chongqing, Tian, Jiang

PA Tianjin Institute of Pharmaceutical Research, P.R. Rep. China

PO Peking Shuang Shengong Shuangong Shuangong, App.

COOBY CHINESE

JP Patent

LA Chinese

PAN CNT

FI IN 2006-160203 A 2006-09-17 CN 2006-160203 20060506  
 AB The invention provides new oral nanoparticle formulation of mast of Colloidal emulsion. The method comprises drying edible bird's nest, pulverizing to obtain fine powders (DSB of which can pass through 200-mesh sieve), micronizing the fine powders with a jet mill to obtain nanoparticles (DSB of which have diameter below 500 nm), and manufacturing into tablets, granule or powder. Compared with the conventional emulsion, the nanoparticles have the advantages of high absorption rate and low dosage.

12 NUMBER 19 OF 49 CAPSULE OXYRIGHT 2009 ACS ON STN

AN 2007-172300 CAPSULE

IN 146-125459

TI Tissue-dispersed uniaxial antileukemic powder as agent for halotherapy

IN Gresham, G. S. Nussbaum, S. A.

PA Gresham, Gresham, Russia

PO Russ. 14pp.

COOBY RUSSIAN

JP Patent

LA Russian

PAN CNT

FI IN 2006-160204 A 2006-09-17 IN 2006-160204 20060506  
 AB The claimed powder from uniaxial antileukemic has particle size of 0.1-30  $\mu$ m, contains non-volatile carbon (DSB) in amount of at least 1.0  $\mu$ m based on total carbon content in finished product, particle as agent and salt additive in amount (mass %): solvent 0.0-10.0; salt additive 10-20.0; and balance: powder from uniaxial antileukemic up to 100%. The method for production of ultrafine powder from uniaxial antileukemic includes: wool removing from uniaxial antileukemic of wool, Siberian step, shaped fiber, or remnant; material crushing to produce particles having size of 0-10  $\mu$ m; drying thereof with air flow at 50°C for less; secondary crushing to produce particles having average size of 0.1  $\mu$ m and secondary drying thereof with air flow at the same temperature, addition under stirring of oleic powder with residual humidity of at most 3 mass % into obtained product in amount sufficient for effective product; creating: grinding of obtained mixture in jet mill in presence of salt additive powder to produce ultrafine powder with particle size of 0.1-30  $\mu$ m and humidity of at most 3 mass % followed by prepacking of finished product in vacuum containers. As oleic powder, mixture of salt additive with volatile solvent in ratio 1:1-1.5 having particle size of at most 10  $\mu$ m is used in amount of at least 10 mass % based on mass of grinding material. Agent for halotherapy has contains aqueous-alkali extract from deionized ultrafine powder composition: 0.0000-0.0005 of DSB N powder from uniaxial antileukemic 1.0-10.0; also 20-40.0; and balance water up to 100%. Solution for halotherapy contains DSB N deionized agent 0.0000-0.0005 and balance: water up to 100%.

FI IN 2006-160205 A 2006-09-17 IN 2006-160205 20060506  
 AB The claimed powder from uniaxial antileukemic has particle size of 0.1-30  $\mu$ m, contains non-volatile carbon (DSB) in amount of at least 1.0  $\mu$ m based on total carbon content in finished product, particle as agent and salt additive in amount (mass %): solvent 0.0-10.0; salt additive 10-20.0; and balance: powder from uniaxial antileukemic up to 100%. The method for production of ultrafine powder from uniaxial antileukemic includes: wool removing from uniaxial antileukemic of wool, Siberian step, shaped fiber, or remnant; material crushing to produce particles having size of 0-10  $\mu$ m; drying thereof with air flow at 50°C for less; secondary crushing to produce particles having average size of 0.1  $\mu$ m and secondary drying thereof with air flow at the same temperature, addition under stirring of oleic powder with residual humidity of at most 3 mass % into obtained product in amount sufficient for effective product; creating: grinding of obtained mixture in jet mill in presence of salt additive powder to produce ultrafine powder with particle size of 0.1-30  $\mu$ m and humidity of at most 3 mass % followed by prepacking of finished product in vacuum containers. As oleic powder, mixture of salt additive with volatile solvent in ratio 1:1-1.5 having particle size of at most 10  $\mu$ m is used in amount of at least 10 mass % based on mass of grinding material. Agent for halotherapy has contains aqueous-alkali extract from deionized ultrafine powder composition: 0.0000-0.0005 of DSB N powder from uniaxial antileukemic 1.0-10.0; also 20-40.0; and balance water up to 100%. Solution for halotherapy contains DSB N deionized agent 0.0000-0.0005 and balance: water up to 100%.



L2 NUMBER 24 OF 49 CAPULE COPYRIGHT 2000 ACS ON STN  
 AN 2000-250075 CAPULE  
 TI Method for producing a pharmaceutical aerosol containing bioactive ingredients by using tetrafluoroethylene as dispersant  
 IN Lu, Tiequn; Wang, Jiansen  
 PA Shanghai Sino Pharmaceutical Co., Ltd., Reg. Rep. Chn  
 SO Shanghai Zhongli Chemical Shanghai, 201305  
 JP Patent  
 LA Chinese  
 LA PACT 11  
 PATENT NO. 21290 DATA APPLICATION NO. DATE  
 CN 11215990 A 20000665 CN 2000-1064253 20041118  
 IN 2000-1064253 20000665  
 AB The title pharmaceutical aerosol is made from therapeutic or bioactive ingredients 0.001-1 wt%, tetrafluoroethylene as dispersant as dispersant 1-10 wt%, a propellant (selected from N<sub>2</sub>, O<sub>2</sub>, CO<sub>2</sub>, 1,1,1,2-tetrafluoroethane or CO<sub>2</sub>/C<sub>2</sub>H<sub>2</sub>F<sub>4</sub>/N<sub>2</sub>O) 5-30 wt%, or mixture thereof, 50-90 wt%, and additives including stabiliser 0.1-1 wt%, surfactant 0.001-0.1 wt%, em. or regulator 0.0-5 wt%, taste corrector 0.0-1 wt%, antioxidant 0.1-1 wt%, and anti-static 0.0-1 wt%, by the steps of (1) vacuum drying or drying under heating acid materials of bioactive ingredients, melting due to room temperature, and solvelling with jet mill to give emulsion having a mean grain size of less than 10 μm; (2) developing liquid materials of bioactive ingredients with anhydrous sodium sulphate for at least 24 h; and (3) mixing the above processed bioactive ingredient materials with the dispersant, homogenizing to give intermediate, wrapping the intermediate in a pressure-proof container, mounting valve and sealing, and infilling the propellant. The bioactive ingredients may be selected from therapeutic or diagnostic agent, anti-allergic drug, bronchodilator, antihistamine, anesthetic, etc.

L2 NUMBER 25 OF 49 CAPULE COPYRIGHT 2000 ACS ON STN  
 AN 2000-250075 CAPULE  
 TI Rhodes Technologies: Specialty API manufacturing in a rapidly changing environment  
 AU Banks, Peter J  
 CS Research and Development, Rhodes Technologies, Coventry, RI 02815, USA  
 SO Abstracts of Papers, 2001 ACS National Meeting, Atlanta, GA, United States, March 26-30, 2000 (2000), 2001-011 Publisher: American Chemical Society, Washington, D. C.  
 OO Rhodes Technologies  
 DT Conference, Meeting Abstract (computer optical disk)  
 LA English  
 AB Rhodes Technologies operates a multi-purpose, FDA-registered and DEA-certified plant with a complete range of active pharmaceutical ingredients (API) production capabilities, including process development, synthesis, drying, plus advanced formulations under contract with state-of-the-art wet mills, as well as design from manufacture to market. Rhodes Technologies has very broad capabilities in developing sophisticated chems. and offer confidential production of high purity APIs and finished dosage forms of innovative pharmaceuticals, as well as marketing and sales services, with a specialization in DEA controlled substances.

L2 NUMBER 26 OF 49 CAPULE COPYRIGHT 2000 ACS ON STN  
 AN 2000-250084 CAPULE  
 TI Milling of organic solids to a jet mill. Part 2: Obtaining the validity of the predicted rate of breakage function  
 AU de Vree, Gert; Tromms, Hermann; Passens, Frieda van der; Noord Maarschalk, Gers  
 CS Department of Pharmaceutics, N.V. Organon, Oss, 3540 BE, Netherlands  
 SO Particle & Particle Systems Characterization (2000), Volume Date 2000, 2(1), 1-5, 207  
 OO Organon Pharmaceuticals, ISSN 1094-0466  
 JP Patent  
 LA English  
 AB The particle size distribution of fine chems. in the solid state, like active pharmaceutical ingredients, is often a critical parameter. To achieve the desired particle size distribution, milling of such materials is usually the method of choice. Since these chems. are often extremely valuable, exact optimization of milling is not possible. Therefore, a model to predict the milling conditions has been developed. The model estimates the rate of breakage function, and needs such parameters like hardness and yield strength as input to calculate the rate of breakage function. This paper attempts to check the validity of the model by a series of experiments. The rate of breakage function, as well as the outcomes of the model using five different model compds. has been performed. It appears that the rate of breakage function can be estimated by:  $B = 8.85(\text{cal}/\text{kg} \cdot 10^6 \text{ kJ/m}^3 \text{ kJ/m}^3) \cdot V \cdot K$ . The model is able to rank the compds. by degree of fracture as an effect of milling. It was also possible to perform a quant. prediction of the impact of milling pressure on the milling of beanoil. Finally, it appeared that the prediction of the large particles in the distribution was significantly better than small ones. Because the oversized material is usually the most critical parameter, the conclusion is that the model has considerable practical applicability.  
 RE CNT 8 THERE ARE 8 CITED REFERENCES AVAILABLE FOR THIS RECORD  
 RE CNT 9 ALL CITATIONS AVAILABLE IN THE RE FORMAT

L2 NUMBER 27 OF 49 CAPULE COPYRIGHT 2000 ACS ON STN  
 AN 2000-199523 CAPULE  
 TI Batch grinding kinetics of Ethenamide particles by fluidized-bed jet-milling  
 AU Fakumada, Tadashi; Ohtani, Boris; Shiohara, Kenji  
 CS Bango Pharmaceutical Co., Ltd., Matsuy, Aichi, 444-0854, Japan  
 SO International Journal of Pharmaceutics (2000), 20(1-2), 69-81  
 OO Organon, ISSN 0168-0719  
 JP Journal  
 LA English  
 AB Ethenamide solids as a representative active pharmaceutical ingredient (API) were batch-ground by a fluidized-bed jet-mill which is a relatively new equipment and promising for production in the pharmaceutical field. Thus, the characteristic grinding mechanism was investigated. As a result, the variation of the residual ratio with grinding time after milling was expressed simply by a math. model using only the first-order function, and it was consistent with exptl. data satisfactorily. As the shape of the function was much different from that of isogr. compound and peculiar to API, a cubic function with respect to particle diameter was defined newly and well fitted to the exptl. data. The function was also found to be affected by the operating parameters as the grinding gas pressure, the charge weight of the material, and the linear velocity of the grinding mill. According to the assessments of breakage and the selection functions derived from the first-order function, it was found that the grinding mechanism of Ethenamide particles was related with particle attrition mainly.  
 RE CNT 10 THERE ARE 10 CITED REFERENCES AVAILABLE FOR THIS RECORD  
 ALL CITATIONS AVAILABLE IN THE RE FORMAT



L2 NUMBER 29 OF 49 CAPULE COPYRIGHT 2009 ACS ON STM  
 AN 2006-06123 CAPULE  
 IN 141-00060  
 T1 Influence of nanomechanical crystal properties on the comminution process of nucleotide acids in spiral jet mills  
 AU Shimizu, Sachiyo; Maruyama, Kazuo; Zimmermann, Ingrid  
 CE Institute of Pharmaceutical Technology, University of Wuerzburg, Wuerzburg, Germany  
 SO Journal of Pharmaceutical Sciences and Biopharmaceutics C0800, 45(2), 194-201  
 ODN ODN JPMAC, ISSN 0003-6411  
 PB Elsevier B.V.  
 LA English  
 AB Milling is a common procedure to improve bioavailability of many active pharmaceutical ingredients (APIs), which initially have low solubility in water. But poor micronization can yield an increase in the solubility of particles. Although particle solubilities in desirable for tablet strength in the subsequent formulation process, increased particle solubility can lead to operational difficulties in a milling equipment due to compression of particles inside. In this article, the impact of milling via a fluidized-bed jet-mill on the cohesive strength and interparticle force was studied. Since theobromine was a pharmaceutical model compound. As a result, the particle shape was found to affect both the tensile strength of powder bed and the interparticle cohesive force. A powder bed, having relatively high void fraction by direct tensile test, shows a low correlation between the cohesive force and the particle surface, while powders with low void fraction by diaphragm compression test show a correlation between the cohesive force and the angularity of the particles.  
 RE NT 12 THERE ARE 10 CITED REFERENCES AVAILABLE FOR THIS RECORD  
 ALL CITATIONS AVAILABLE IN THE ISI PFORMAT

L2 NUMBER 29 OF 49 CAPULE COPYRIGHT 2009 ACS ON STM  
 AN 2006-06123 CAPULE  
 IN 141-00060  
 T1 Variation in particle shape of active pharmaceutical ingredients prepared by fluidized-bed jet-milling  
 AU Fukushima, Tadashi; Kawaguchi, Kohji; Ichino, Ryoji; Shimohara, Kazuo  
 CE Chugai Pharmaceutical Co., Ltd., 3-9-1 Kanematsu, Bunkyo City, 464-0603, Japan  
 SO Yakugaku Zasshi C0800, 125(12), 961-967  
 ODN ODN YJZAS, ISSN 0003-6546  
 PB Pharmaceutical Society of Japan  
 LA Japanese  
 AB In pharmaceutical industries, most active pharmaceutical ingredients are poorly water soluble, and therefore milling processes are important to obtain fine particles that can be easily dissolved in the body. However, the main purpose of milling is micronization of particles, from the viewpoint of fine particle preparation in the formulation process, milling has not been investigated sufficiently. In this paper, theobromine was milled under various operating conditions using a fluidized-bed jet-mill. It was found that not only the particle size but also the particle shape varied with the milling conditions. The relationship between particle shape and milling conditions has been obtained expli-

L2 NUMBER 31 OF 49 CAPULE COPYRIGHT 2009 ACS ON STM  
 AN 2006-06169 CAPULE  
 IN 141-02791  
 T1 Microcrystals of 3-(3'-O-4,4'-dimethoxystyryl)-1,3,5-trimethyl-7,8-dihydro-1H-purine-2,6-dione  
 AU Bando, Kazutoshi; Aoki, Noriaki; Ohsaki, Toshiro; Idehira, Akihiko; Ishikawa, Toshiro; Kiguchi, Ryoichi; Inayama, Eiji; Asanome, Kazuo  
 CE Eryu Sakai Kogyo Co., Ltd., Japan  
 SO J. Pharm. Sci., 22(2)  
 ODN ODN JPS, ISSN 0022-0549  
 PB Wiley-Liss, Inc  
 LA English  
 AB Milling is a common procedure to improve bioavailability of many active pharmaceutical ingredients (APIs), which initially have low solubility in water. But poor micronization can yield an increase in the solubility of particles. Although particle solubilities in desirable for tablet strength in the subsequent formulation process, increased particle solubility can lead to operational difficulties in a milling equipment due to compression of particles inside. In this article, the impact of milling via a fluidized-bed jet-mill on the cohesive strength and interparticle force was studied. Since theobromine was a pharmaceutical model compound. As a result, the particle shape was found to affect both the tensile strength of powder bed and the interparticle cohesive force. A powder bed, having relatively high void fraction by direct tensile test, shows a low correlation between the cohesive force and the particle surface, while powders with low void fraction by diaphragm compression test show a correlation between the cohesive force and the angularity of the particles.  
 RE NT 6 THERE ARE 10 CITED REFERENCES AVAILABLE FOR THIS RECORD  
 ALL CITATIONS AVAILABLE IN THE ISI PFORMAT

L2 NUMBER 31 OF 49 CAPULE COPYRIGHT 2009 ACS ON STM  
 AN 2006-06169 CAPULE  
 IN 141-02791  
 T1 Microcrystals of 3-(3'-O-4,4'-dimethoxystyryl)-1,3,5-trimethyl-7,8-dihydro-1H-purine-2,6-dione  
 AU Bando, Kazutoshi; Aoki, Noriaki; Ohsaki, Toshiro; Idehira, Akihiko; Ishikawa, Toshiro; Kiguchi, Ryoichi; Inayama, Eiji; Asanome, Kazuo  
 CE Eryu Sakai Kogyo Co., Ltd., Japan  
 SO J. Pharm. Sci., 22(2)  
 ODN ODN JPS, ISSN 0022-0549  
 PB Wiley-Liss, Inc  
 LA Japanese  
 AB Milling is a common procedure to improve bioavailability of many active pharmaceutical ingredients (APIs), which initially have low solubility in water. But poor micronization can yield an increase in the solubility of particles. Although particle solubilities in desirable for tablet strength in the subsequent formulation process, increased particle solubility can lead to operational difficulties in a milling equipment due to compression of particles inside. In this article, the impact of milling via a fluidized-bed jet-mill on the cohesive strength and interparticle force was studied. Since theobromine was a pharmaceutical model compound. As a result, the particle shape was found to affect both the tensile strength of powder bed and the interparticle cohesive force. A powder bed, having relatively high void fraction by direct tensile test, shows a low correlation between the cohesive force and the particle surface, while powders with low void fraction by diaphragm compression test show a correlation between the cohesive force and the angularity of the particles.  
 RE NT 12 THERE ARE 10 CITED REFERENCES AVAILABLE FOR THIS RECORD  
 ALL CITATIONS AVAILABLE IN THE ISI PFORMAT

RE NT 12 THERE ARE 10 CITED REFERENCES AVAILABLE FOR THIS RECORD  
 ALL CITATIONS AVAILABLE IN THE ISI PFORMAT

L2 NUMBER 35 OF 49 CAPULE COPYRIGHT 2009 ACS ON STN  
AN 2004-126503 CAPULE

IN 143-112109

TI Bepato-protective effects of amorphous and nano-particle preparations of ursodeoxycholic acid on CCl<sub>4</sub>-induced mice: effects of three types of fine grinding mills

AB Chang, Min, Yang, Joon, Lee, J, Hyoun, Kim, He, Jo, Park, The, Hyun, Chang, Han, Young, Kim, Yoo, Jung, Beak, Seung, Shin, Kim, Hyun, Yi, Choi, Woo, Shik

CI Interdisciplinary Program in Fooder Technology, Graduate School, Pusan National University, Pusan, 600-739, S. Korea

DO Journal of Applied Pharmacology (JGAP), 2003, 1-6

IN JGAP 100466-1204 1225-4710

PS Korean Society of Applied Pharmacology

PT Journal

LA Korean

AB

The particle size of medicinal materials is an important phys. property that affects the pharmaceutical behaviors such as dissoln., chemical stability, and bioavailability of solid dosage forms. The size reduction of raw medicinal powder is needed to formulate small drugs or slightly soluble medicines and to improve the pharmaceutical properties such as the solubility, the pharmaceutical mixing, and the dispersion. The ob. active of the present study is to evaluate physical activity of amorphous and nano-particle prepns of insol. drug, ursodeoxycholic acid (UDCA), which were made by three types of (fine grinding) mills. The change of phys. properties of ground UDCA was confirmed by Water-soluble extraction and X-ray diffraction. We have investigated hepatoprotective effects of the nano-particle prepns of UDCA by placentary cells, vibration rod mill and jet mill. In CCl<sub>4</sub>-induced oxidatively injured mouse liver, the results showed that nano-particle prepns of UDCA all decreased reactive oxygen species generation and lipid peroxidation. In CCl<sub>4</sub>-induced oxidative stress mice, more than, nano-particle prepns, by vibration rod mill and jet mill showed more significant hepatoprotective effects compared to intact UDCA and placentary mill-ground UDCA. These results suggest that ground UDCA with vibration rod mill and jet mill shows a high amorphous state and the improved dissoln.

L2 NUMBER 35 OF 49 CAPULE COPYRIGHT 2009 ACS ON STN  
AN 2004-126503 CAPULE

IN 143-112109

TI Methods and apparatus for making particles using spray dryer and in-line jet mill

AB Chatterjee, Donald B., Narasimhan, Sridhar, Altmeppen, David, Koschek, Paul, Sengupta, Mark, Joshi, Julie A., Bernstein, Howard

CI Acushnet, Inc., USA

DO U.S. Pat. Appl. Publ., 19 pp.

IN US2004-123309

PT Patent

LA English

AB

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI US 2004/018007	A1	2004/06/04	US 2000-024943	2002/12/19
US 2004/018007	B2	2004/11/04		
CA 2511238	A1	2004/06/22	CA 2000-024943	2002/12/19
WO 2000/009047	A1	2000/02/02	WO 2000-023709	2000/12/10
#	AC	AC	AC	AC
CA	CA	CA	CA	CA
CH	CH	CH	CH	CH
CN	CN	CN	CN	CN
DE	DE	DE	DE	DE
DK	DK	DK	DK	DK
EA	EA	EA	EA	EA
ES	ES	ES	ES	ES
FI	FI	FI	FI	FI
FR	FR	FR	FR	FR
GB	GB	GB	GB	GB
GR	GR	GR	GR	GR
HK	HK	HK	HK	HK
IL	IL	IL	IL	IL
IN	IN	IN	IN	IN
JP	JP	JP	JP	JP
KE	KE	KE	KE	KE
KR	KR	KR	KR	KR
LT	LT	LT	LT	LT
LU	LU	LU	LU	LU
MA	MA	MA	MA	MA
MC	MC	MC	MC	MC
MD	MD	MD	MD	MD
ME	ME	ME	ME	ME
MG	MG	MG	MG	MG
MI	MI	MI	MI	MI
ML	ML	ML	ML	ML
MM	MM	MM	MM	MM
MN	MN	MN	MN	MN
MO	MO	MO	MO	MO
MP	MP	MP	MP	MP
MQ	MQ	MQ	MQ	MQ
MR	MR	MR	MR	MR
MS	MS	MS	MS	MS
MT	MT	MT	MT	MT
MU	MU	MU	MU	MU
MX	MX	MX	MX	MX
MY	MY	MY	MY	MY
NZ	NZ	NZ	NZ	NZ
OM	OM	OM	OM	OM
PA	PA	PA	PA	PA
PE	PE	PE	PE	PE
PG	PG	PG	PG	PG
PH	PH	PH	PH	PH
PK	PK	PK	PK	PK
PL	PL	PL	PL	PL
PT	PT	PT	PT	PT
RU	RU	RU	RU	RU
SA	SA	SA	SA	SA
SC	SC	SC	SC	SC
SD	SD	SD	SD	SD
SE	SE	SE	SE	SE
SG	SG	SG	SG	SG
SI	SI	SI	SI	SI
SK	SK	SK	SK	SK
SL	SL	SL	SL	SL
SM	SM	SM	SM	SM
SN	SN	SN	SN	SN
SO	SO	SO	SO	SO
SR	SR	SR	SR	SR
SS	SS	SS	SS	SS
ST	ST	ST	ST	ST
SV	SV	SV	SV	SV
SW	SW	SW	SW	SW
SY	SY	SY	SY	SY
SZ	SZ	SZ	SZ	SZ
TC	TC	TC	TC	TC
TD	TD	TD	TD	TD
TE	TE	TE	TE	TE
TF	TF	TF	TF	TF
TG	TG	TG	TG	TG
TH	TH	TH	TH	TH
TJ	TJ	TJ	TJ	TJ
TL	TL	TL	TL	TL
TM	TM	TM	TM	TM
TN	TN	TN	TN	TN
TO	TO	TO	TO	TO
TR	TR	TR	TR	TR
TT	TT	TT	TT	TT
TU	TU	TU	TU	TU
TV	TV	TV	TV	TV
UA	UA	UA	UA	UA
UG	UG	UG	UG	UG
US	US	US	US	US
UY	UY	UY	UY	UY
UZ	UZ	UZ	UZ	UZ
VC	VC	VC	VC	VC
VE	VE	VE	VE	VE
VG	VG	VG	VG	VG
VI	VI	VI	VI	VI
VN	VN	VN	VN	VN
VS	VS	VS	VS	VS
YT	YT	YT	YT	YT
ZA	ZA	ZA	ZA	ZA
ZB	ZB	ZB	ZB	ZB
ZC	ZC	ZC	ZC	ZC
ZD	ZD	ZD	ZD	ZD
ZE	ZE	ZE	ZE	ZE
ZF	ZF	ZF	ZF	ZF
ZG	ZG	ZG	ZG	ZG
ZH	ZH	ZH	ZH	ZH
ZI	ZI	ZI	ZI	ZI
ZJ	ZJ	ZJ	ZJ	ZJ
ZK	ZK	ZK	ZK	ZK
ZL	ZL	ZL	ZL	ZL
ZM	ZM	ZM	ZM	ZM
ZN	ZN	ZN	ZN	ZN
ZO	ZO	ZO	ZO	ZO
ZZ	ZZ	ZZ	ZZ	ZZ

AB Methods and apparatus are provided for making particles comprising: (a) spraying an emulsion, solution, or suspension, which comprises a solvent and a bulk material (e.g., a pharmaceutical agent), through an atomizer and into a primary drying chamber, having a drying gas flowing through it, to form droplets comprising the solvent and bulk material (dispersed in the drying gas); (b) evaporating, in the primary drying chamber, at least a portion of the solvent into the drying gas to solidify the droplets and form particles dispersed in drying gas; and (c) flowing the particles and at least a portion of the drying gas through a jet mill to deagglomerate or grind the particles. By coupling spray drying with in-line jet milling, a single step process is created from two sep. unit operations; and an in-line collection step is advantageously eliminated. The in-line process has further

L2 NUMBER 35 OF 49 CAPULE COPYRIGHT 2009 ACS ON STN (Continued)  
ABSTRACTS IN TIME AND COST OF PROCESSING

RE CNT 49 1235 LBS 43 CITED REFERENCES AVAILABLE FOR THIS RECORD

ALL CITATIONS AVAILABLE IN THIS DOCUMENT

L2 NUMBER 35 OF 49 CAPULE COPYRIGHT 2009 ACS ON STN  
AN 2004-123309 CAPULE

IN 143-112109

TI R & D of milling technology in pharmaceutical industry

AB Fukushima, Tadashi, Tom, Jun, B

CI Process R & D Lab., Sanofi Pharmaceutical Co., Ltd., Musashi, 444-0658, Japan

DO Patent Kokusai Kinshi (PCT), 40/09, 655-463

IN PCT/JP2004-008415

PT Patent

LA Japanese

AB

In the pharmaceutical industry, milling process is important to improve the solubility of the bulk drug by grinding them into the small particle size. Small particles as the bulk drug help patients to be easily dissolved in their body, because most of them have very low solubility. However, the grinding characteristics and scale-up methodologies of ordinary miller techniques for pharmaceutical compounds have hardly ever been reported. Five kinds of milling techniques (jet-mill, fluidized jet-mill, air-mill, comminutor, and cavitation-mill) for the drug W-1, which we have developed, were evaluated on the basis of the particle size of the milled material and the durability and the scale-up ability of these techniques. From our study, the fluidized jet-mill can be found to obtain the finest particle in size and the cheapest technique and show the most durability. The scale-up number,  $N_s$ , derived from the dynamic balance of a centrifugal classifier was defined as the scale-up factor and its application-ability was also evaluated using the larger scale equipment.





12 ANWER 41 OF 49 CAPULE OFFRIGHT 2009 ACS on STN

AK 1596-38122 CAPULE

IN 159-9474

ORIP 159-16536A,16642a

TI Method for dissolving lipophilic material

IN Tada, Atsushi; Miyake, Tsumotohi; Tanaka, Tsumoto; Miyake, Fumeteri; Hiki,

Kenzo; Watan, Katsuhiko; Haraoka, Kenji

PA Sanzoku Sugar Refining Co., Ltd., Japan; Genosa K. K.; Hakusai Chem

Industry, Ltd.

50 Jpn. Kohai Tokyo Kobo, 20 pp

ORIP 159-16536A

TI Patent

LA Japanese

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

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LA Patent

12 ANWER 42 OF 49 CAPULE OFFRIGHT 2009 ACS on STN

AK 1596-62190 CAPULE

IN 159-23777

ORIP 159-47858A, 47858B

TI Tablets or granules containing Chlorella powder

IN Maruyama, Isao; Nakao, Takahiko; Tanaka, Yoshinaka; Ando, Yotaro

PA Chlorella Ind., Japan

50 Jpn. Kohai Tokyo Kobo, 4 pp

ORIP 159-47858A

TI Patent

LA Japanese

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

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12 ANWER 43 OF 49 CAPULE OFFRIGHT 2009 ACS on STN (Continued)

example, 10 parts insulin was dispensed in third water and 4 parts No  
tunocholate (absorption enhancer) was added. Melitane 84 parts was  
added to the above mixt. and pH was adjusted to 7.4. The soln was cond.  
by evapn. of the water and the obtained solid cake was crushed, sieved,  
and micronized in a jet mill. The micronized powder was  
suspensionized and filled into a dry powder inhaler.

RE. CNT. 5. THERE ARE 5 CITED REFERENCES AVAILABLE FOR THIS RECORD

ALL CITATIONS AVAILABLE IN THE RE. FURTHER

12 ANWER 44 OF 49 CAPULE OFFRIGHT 2009 ACS on STN

AK 1596-47858A CAPULE

IN 159-12378

ORIP 159-23852A, 23852B

TI Powder formulations containing melitane as a diluent

IN Baerentzen, Kalli; Johansson, Ann; Lindén, Helena

PA Astra-Meriebolog, Sweden

50 PCT Int. Appl., 21 pp

ORIP 159-23852A

TI Patent

LA Swedish

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

LA Patent

FI Patent

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LA Patent

FI Patent

LA Patent

AS A powder formulation for the administration of medically useful  
polypeptides, comprises the polypeptides with melitane as diluent. For

12 NUMBER 44 OF 49 CAPULE COPYRIGHT 2009 ACS ON STM  
 AN 1990-208121 CAPULE  
 IN 134-250406  
 ORIP 134-543274, 543506  
 TI Method of milling  
 IN Baflova, Andrew John  
 S Afr.  
 SO 5 African, 17 pp.  
 COOIN 77XK43  
 DE Patent  
 LA English  
 PAN CNT 1

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
FI 04000425	A	19940609	04 1990-0649	19951104
JP 04263112	A	19940610	JP 1990-204837	19951125
FR02 1990-0696	A	19901125		

AB The milling of a particulate material comprises passing a gas (steam or air) through a jet mill while feeding the particulate material. An drying pigment, an organic-colored pigment or a pharmaceutical composition from a hollow vessel containing the material through an inlet to be entrained by the gas and passing the mixture of gas and entrained particles as formed into the jet mill. The amount of particulate material in the hollow vessel is insufficient to fill the vessel thus creating an inflow and a gas is maintained in the inflow at a pressure of 30-60 MPa above atmospheric pressure but less than the pressure at which gas is introduced to the jet mill.

12 NUMBER 46 OF 49 CAPULE COPYRIGHT 2009 ACS ON STM  
 AN 1990-208919 CAPULE  
 IN 134-250406  
 ORIP 134-543274, 543506  
 TI Liposome powders for pharmaceutical compositions  
 IN Schreyer, Jane  
 PA Advanced Therapeutics, Inc., USA  
 PCT Int. Appl., 17 pp.  
 COOIN 77XK22  
 DE Patent  
 LA English  
 PAN CNT 1

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
FI 90428976	A	19941222	90 1990-126137	19940831
JP 04 1990-122584	A	19920607		

AB A procedure for producing dry liposome powders (to improve their stability) which can be formulated into a variety of pharmaceutical forms involves micronizing lyophilized liposome cakes with a jet mill or other device to generate dry powders with a diameter of 1-100  $\mu$ m. Nine grams water phosphatidylcholine (118 mg) were dispersed in 100 ml aqueous solution containing 8 g lactose (945 mg). Liposomes were introduced through a polysorbate membrane and lyophilized. The lyophilized cake was stirred into a jet mill and the mill operated under N<sub>2</sub> so as to minimize potential oxidative and absorption of water. Liposomes were milled for 3 min at an inlet pressure of 40 psig. A majority of the mass introduced into the jet mill was collected in the cyclone of the mill representing a particle size of 6-10  $\mu$ m diameter. These powders could be introduced into capsules or used as powder tablets.

RE CNT 6 THERE ARE 6 CITED REFERENCES AVAILABLE IN THIS RECORD  
 ALL CITATIONS AVAILABLE IN THE HS 900047

12 NUMBER 45 OF 49 CAPULE COPYRIGHT 2009 ACS ON STM  
 AN 1990-270016 CAPULE  
 IN 134-251717  
 ORIP 134 190024, 180646

TI Improvement of dissolution characteristics of a new chalcone derivative, SP-740: comparison between side reduction, solid dispersion and inclusion complexation  
 IN Ito, Shunji; Demachi, Miki; Toriomi, Tomoko; Adachi, Takeshi; Imai, Shiroto; Hirayama, Fumihiko; Nakano, Kazuo  
 CS Research Center, Taisyo Pharmaceutical Co., Ltd., Saitama, 330, Japan  
 Chemical & Pharmaceutical Bulletin (1996), 45(12), 2221-6  
 COOIN 197AAL 1238 0009-2343  
 DE Patent  
 LA Japanese  
 PAN CNT 1

AB Three pharmaceutical techniques, i.e., size-reduction, solid dispersion and inclusion complexation, were employed for improvement of the dissolved rate of 1-(tert-butyl-2'-carboxymethyl-4'-O-methyl-2'-hydroxyethyl)chalcone (SP-740). For the size reduction, pulverization was performed using a jet mill. The solid dispersions of SP-740 were prepared with polyethylene glycol 4000 and polyvinylpyrrolidone K60/5. The inclusion complexes of SP-740 with 5 natural cyclodextrins ( $\alpha$ -,  $\beta$ -,  $\gamma$ -CDs) were prepared by the freeze-drying method, or they were isolated according to the Be type phase-solubility diagram. The dissolved rates of SP-740 from the PVP copolymer, the P-CD complex were much larger than that of the size-reduced form. On concentrated storage (40% and 70% relative humidity) for 1 mo, the PVP copolymer showed a decrease in the dissolved rate and a change in appearance, whereas the P-CD complex showed no changes. The inclusion complexation is preferable among the 5 techniques employed for improving of the dissolved rate of SP-740.

12 NUMBER 47 OF 49 CAPULE COPYRIGHT 2009 ACS ON STM  
 AN 1990-208709 CAPULE  
 IN 134-250406  
 ORIP 134-543274, 543506  
 TI Pharmaceutical compositions containing micronized siroquin  
 IN Pakete, Paul; Benesch, Dennis; Simons, Latvian; Marmody, Shiroka, Zborovska, Katalin; Tombo, James  
 PA BDII Oxygentec, Hong.  
 DE Pat. Int. Appl., 17 pp.  
 COOIN 77XK26  
 DE Patent  
 LA English  
 PAN CNT 1

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
FI 92254307	A	19960602	GB 1989-012086	19910207
DE 2254307	B	19960610		
DE 61145	C2	19960628	DE 1989-0621	19951008
DE 200628	B	19960628		
JP 04173949	A	19960628	JP 1989-270631	19910219
CA 2001673	CA	19960628	CA 1989-2000473	19910207
FR 2638357	A	19960604	FR 1989-1117	19910207
FR 2638357	B	19961027		
IL 61118	A	19960606	IL 1989-01158	19910207
DE 2566112	A1	19960631		
DE 2566112	C2	19960631	DE 1989-056612	19910500

AB The present invention relates to an oral pharmaceutical composition comprising piroquin as active ingredient and lactose as a carrier in micronized form, i.e. 500  $\mu$ m of the composition has a particle size <20  $\mu$ m. The composition may be made up into tablets and capsules. The preparation containing the micronized piroquin crystals allows the desired dissolution rate and the scattering of the active ingredient content. Thus, piroquin 200, micronized 200, and micronized 200 g were mixed and micronized in Type 30-30 air-jet mill by adjusting the air value to 6 bar. Lactose 2000 and Na lauryl sulfate 5.6 g were homogenized and triturated; the above micronized powder, triturated powder, lactose 500, corn starch 130 g, and Mg stearate 0.3 g were totally mixed, homogenized, and formed into capsules and tablets.

L2 ANSWER 49 OF 49 CAPLIC COPYRIGHT 2009 ACS on STM  
AN 1266 46155 CAPLIC

IN 110-51994

ORIP 110-47914,47946

T1 Morphic features variation of solid particles after size reduction:

AB Thibert, R.; Akbari, M.; Tawab, A.

CS Fac. Pharm., Univ. Montreal, Montreal, QC, Can.

SO International Journal of Pharmaceutics 11960, 47(1-3), 171-7

OSON 119106, ISSN 0269-4727

JF Journal

JA English

AS Fourier descriptors of the contours were used to evaluate the effect of

size reduction and jet mill grinding on particle shape.

While jet mill grinding produced particles with

smoother boundary, less elongation and higher degree of roundness,

size reduction yielded fragments closer in shape to the original crystal

data obtained suggest that the morphic features of daughter fragments are

determined mainly by the mechanism of size reduction and material structure

L2 ANSWER 49 OF 49 CAPLIC COPYRIGHT 2009 ACS on STM  
AN 1266 46155 CAPLIC

IN 110-51994

ORIP 110-47914

T1 Milling in air-pressure centrifugal mills

AB Lewandowski, Marcin

CS Inst. Chem. Res. Autom., Acad. Chem. Res., Krakow, Pol.

SO Ingenieria i. Analiza Chemiczna 11910, 14(1), 24-7

OSON 119106, ISSN 0046-0607

JF Journal

JA Polish

AS Air jet mills were examined for milling

various inorg. substances. The 3 types investigated had milling

chamber diam. 100, 200, and 400 mm and capacities 10, 60, and 150 kg/hr.,

resp. They were superior to other mills with regard to homogeneity, very

small particle product size, and contamination. The advantage of

jet mills is apparent especially when using hot gas or steam.

The latter also enables operation under sterile conditions, which makes it

suitable for pharmaceuticals

=> => d que 110 stat

L3	5	SEA	FILE=CAPLUS	ABB=ON	PLU=ON	"IZAWA NAOTO"/AU
L4	1	SEA	FILE=CAPLUS	ABB=ON	PLU=ON	"SATOH NORIE"/AU
L5	35	SEA	FILE=CAPLUS	ABB=ON	PLU=ON	"YAGI NOBUHIRO"/AU
L6	3	SEA	FILE=CAPLUS	ABB=ON	PLU=ON	"OUCHI KAZUE"/AU
L7	6	SEA	FILE=CAPLUS	ABB=ON	PLU=ON	"NARITA SHOICHI"/AU
L8	27	SEA	FILE=CAPLUS	ABB=ON	PLU=ON	"AOKI NOBORU"/AU
L9	70	SEA	FILE=CAPLUS	ABB=ON	PLU=ON	L3 OR L4 OR L5 OR L6 OR L7 OR
	L8					
L10	2	SEA	FILE=CAPLUS	ABB=ON	PLU=ON	L9 AND (MICROCRYSTAL?)

=> d 1-2 bib abs





=> s l9 and (pulveriz? or mill? or powder?)

86272 PULVERIZ?

320743 MILL?

757581 POWDER?

202341 POWD

255 POWDS

202468 POWD

(POWD OR POWDS)

878907 POWDER?

(POWDER? OR POWD)

L11 8 L9 AND (PULVERIZ? OR MILL? OR POWDER?)

=> d 1-8 bib abs

L21 ANSWER 2 OF 8 CAPULE COPYRIGHT 2009 ACS ON STN  
 AN 2004 996180 CAPULE  
 IN 14142700  
 TN Mineral salts of (S)-8-(3,4-dimethoxystyryl)-1,3,5-triethyl-2,7-  
 dihydro-1H-pyrazine-2,6-dione  
 EN Korea, Kazakhstan, Aki, Notozu, Ochiai, Toshio, Behoda.  
 RU Japan, Ishikawa, Yamori, Egiuchi, Matsuo, Hayakawa, Eiji; Asanome,  
 Kazuo  
 PA Kowa Yakko Kogyo Co. Ltd., Japan  
 FO PCT Int. Appl., 22 pp.  
 RU62004 000000 PCTRU  
 DT Patent  
 LA Japanese  
 PAM CNT 1

[illegible]

EN	ANWER, G. & F. CAPLUS. COPYRIGHT 2000 AS ON STN
AN	0002: 0007678
IN	130-41636
TI	Stabilization of phosphate degradable drug powder by dry coating
AB	agglomerates
AU	En, Ryumai; Maeda, Akio; Shinohara, Kenji; Iwano, Naoto; Naka-
CG	Yoshioka, Shoji. <i>Int. J. Pharm.</i> , 1999, 184, 2, 199-207, 29 refs.
PU	Japan; Kinki Kagaku Ind. Co. Ltd., 330-333
PI	Patent; Kinki Kagaku Ind. Co. Ltd., 0306-4107
PS	Patent; Kinki Kagaku Ind. Co. Ltd.
PT	Japanese
LA	Japanese
AB	Phosphate degradable drug powder was stabilized by dry coating drug agglomerates with UV protective powder with a high-shear mixer. As an example, a phosphate degradable drug powder was stabilized with UV protective powder and titanium dioxide (TiO <sub>2</sub> ) as a protective one. The drug forms a subcoated under UV irradiation and the amount of the component of UV protective powder was 10-20% by weight. The result of the protective performance improved with the mass ratio of TiO <sub>2</sub> to the component of UV protective powder and the amount of the component of UV protective powder to PLG, the



=> d his full

(FILE 'HOME' ENTERED AT 12:39:26 ON 23 MAR 2009)

FILE 'CAPLUS' ENTERED AT 12:39:37 ON 23 MAR 2009

L1 14734 SEA ABB=ON PLU=ON (PHARMACEUTICAL OR PHARMACEUTICALS) (L) (PULV  
L2 ERIZE OR PULVERIZATION OR MILLING OR (JET MILL) OR POWDER)  
49 SEA ABB=ON PLU=ON L1 AND (JET MILL)  
D QUE L2 STAT  
D 1-49 BIB ABS  
E IZAWA NAOTO/AU  
L3 5 SEA ABB=ON PLU=ON "IZAWA NAOTO"/AU  
E SATOH NORIE/AU  
L4 1 SEA ABB=ON PLU=ON "SATOH NORIE"/AU  
E YAGI NOBUHIRO/AU  
L5 35 SEA ABB=ON PLU=ON "YAGI NOBUHIRO"/AU  
E OUCHI KAZUE/AU  
L6 3 SEA ABB=ON PLU=ON "OUCHI KAZUE"/AU  
E NARITA SHOICHI/AU  
L7 6 SEA ABB=ON PLU=ON "NARITA SHOICHI"/AU  
E AOKI NOBORU/AU  
L8 27 SEA ABB=ON PLU=ON "AOKI NOBORU"/AU  
L9 70 SEA ABB=ON PLU=ON L3 OR L4 OR L5 OR L6 OR L7 OR L8  
L10 2 SEA ABB=ON PLU=ON L9 AND (MICROCRYSTAL?)  
D QUE L10 STAT  
D 1-2 BIB ABS  
L11 8 SEA ABB=ON PLU=ON L9 AND (PULVERIZ? OR MILL? OR POWDER?)  
D 1-8 BIB ABS

10/582,328 03/23/2009

Page 22

FULL ESTIMATED COST	241.80	242.02
DISCOUNT AMOUNTS (FOR QUALIFYING ACCOUNTS)	SINCE FILE	TOTAL
CA SUBSCRIBER PRICE	ENTRY	SESSION
	-48.38	-48.38

STN INTERNATIONAL LOGOFF AT 13:03:42 ON 23 MAR 2009